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| Author(s)    | Nakamoto, Masashi; Miyabayashi, Yoshitugu;<br>Holappa, Lauri et al.                     |
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# A Model for Estimating Viscosities of Aluminosilicate Melts Containing Alkali Oxides

Masashi NAKAMOTO, 1) Yoshitugu MIYABAYASHI, 2) Lauri HOLAPPA 1) and Toshihiro TANAKA 3)

- 1) Laboratory of Metallurgy, Helsinki University of Technology, P.O. Box 6200, FI-02015 TKK, Espoo, Finland.
- 2) Nikko Environmental Services Co., Ltd., 3453 Miyata, Hitachi, Ibaraki 317-0055 Japan.
- 3) Division of Materials and Manufacturing Science, Osaka University, 2-1 Yamadaoka, Suita, Osaka 565-0871 Japan.

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A model to estimate the viscosity of aluminosilicate melts, including alkali oxides, was constructed in the present study. The model is based on an earlier model, and considers the bonding state of oxygen in molten silicate and the flow mechanism of melts with a network structure. The straightforward method of Susa *et al.* to evaluate bonding states of oxygen in chemical compositions was applied to the present model since their method can easily be extended to any multi-component system. The calculation results of our model can express the dependence on viscosity in quaternary aluminosilicates containing alkali oxide and their subsystems.

KEY WORDS: viscosity; silicate melts; structure; aluminosilicate melts; alkali oxides.

# 1. Introduction

Demand of smelting furnaces for waste treatment has been increasing in the respect of detoxification as well as recycling of industrial waste such as asbestos, 1,2) shredder residue, 1,3,4) and glass dust containing lead. 5) The essential issue in smelting furnace operations is to elucidate adequate conditions with the aim of stabilizing processes due to the wide variety in the composition of industrial waste. In this regard, Miyabayashi et al. 1) pointed out that the fluidity of slag is one of the crucial operating components. Although the fluidity of slag is typically evaluated by the viscosity measurement, the estimation of viscosity by models is considered to be much more helpful in evaluating viscosity in case of melting furnaces. This is because of the considerable difficulty in measuring viscosity of all kinds of slags in melting furnaces due to the diversity in composition of industrial waste. The system of the slag in melting furnaces for the waste including asbestos is the multi-component aluminosilicate containing CaO, FeO, Fe<sub>2</sub>O<sub>3</sub>, MgO,

Many models to estimate the viscosity of slag melts have been developed in the past.<sup>6-8)</sup> It has been accepted that the estimation of viscosity of molten slags is a difficult task since the abrupt and complicated structure changes of silicate melts are reflected by the viscosity. From this viewpoint, successful models based on the structure of molten slags have been proposed by Zhang and Jahanshahi,<sup>9-11)</sup> and Kondratiev and Jak.<sup>12-15)</sup> The three bonding states of oxygen in slag melts, which are (i) bridging oxygen, (ii) non-bridging oxygen ion, and (iii) free oxygen ion, are considered in their viscosity model. The authors<sup>16-21)</sup> have also constructed a structurally-based viscosity model by consid-

ering the flow mechanism of silicate melts within the network structure as well as the bonding states of oxygen in molten silicate. In this model, the concentrations of non-bridging oxygen ions and free oxygen ions are calculated as bonding states of oxygen by the IRSID thermodynamic 'cell model.' <sup>22,23)</sup> This viscosity model can represent the composition dependence of viscosity in a wide composition range in the multi-component silicate system SiO<sub>2</sub>–CaO–MgO–FeO–Al<sub>2</sub>O<sub>3</sub> in blast furnace process. However, the IRSID "cell model" is not applicable to slag containing alkali oxides, which cannot be ignored in the slag of melting furnace, in spite of its wide validity system SiO<sub>2</sub>–TiO<sub>2</sub>–Ti<sub>2</sub>O<sub>3</sub>–Cr<sub>2</sub>O<sub>3</sub>–Al<sub>2</sub>O<sub>3</sub>–Fe<sub>2</sub>O<sub>3</sub>–CrO–FeO–MgO–MnO–CaO–CaF<sub>2</sub>–S.

On the other hand, a predictive equation for the refractive indices of aluminosilicate melts was proposed by Susa et al.<sup>24)</sup> Assuming that the structure of aluminosilicate melts consists of only three kinds of chemical bonds, i.e. Si-BO (bridging oxygen in Si tetrahedral unit), Al-BO (bridging oxygen in Al tetrahedral unit with a charge-compensating cation), and Si-NBO (NBO: non-bridging oxygen connected with Si) with a charge-compensating cation, it is possible to calculate the bonding states of oxygen in molten aluminosilicate by the chemical composition of slag without any thermodynamic parameters. Owing to a simple method, the evaluation of the bonding states of oxygen can be conducted in various kinds of silicate systems including alkali oxides as well as alkaline earth oxides. Their equation succeeds in predicting the refractive index values with small error in six component silicate melts in spite of its simplicity.

In the present work, the earlier viscosity model developed by the authors was modified to the viscosity of alumi-

nosilicate melts containing alkali oxides in melting furnaces, SiO<sub>2</sub>–CaO–MgO–FeO–K<sub>2</sub>O–Na<sub>2</sub>O–Al<sub>2</sub>O<sub>3</sub> system, by applying the method of Susa *et al.* to evaluate the bonding states of oxygen in the molten silicate instead of thermodynamic models.

#### 2. Model

# 2.1. Equation

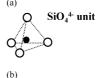
The equation to describe the viscosity of molten silicate slag in the present model is based on the equation in the earlier model which was proposed considering the bonding state of oxygen in the network structure of silicate melts and its flow mechanism. 16-21) The concept of the model is as follows: Silicate slag has a network structure made of bonding SiO<sub>4</sub><sup>4-</sup> units and Si tetrahedral ions, as shown in Fig. 1(a). Si tetrahedral ions are combined through bridging oxygen O<sup>0</sup>, the convex oxygen in the structure of Si tetrahedral ions. The non-bridging oxygen ion O and the free oxygen ion O<sup>2-</sup> are generated by partially cutting off the network structure of Si tetrahedral in SiO2 when adding some basic oxides such as CaO and Na2O in silicate slag, as shown in Fig. 1(b). The non-bridging oxygen ion and the free oxygen ion have a larger mobility than the bridging oxygen in the network structure because there are "cuttingoff" points. These are bonds of oxygen not connected to Si, just next to the non-bridging oxygen ion and the free oxygen ion due to the breaking of the network structure. Assuming that the movements of "cutting-off" points cause a viscous flow, therefore, an increase in the number of nonbridging oxygen ions and free oxygen ions yields a lowering of the activation energy of viscosity. In addition, it is assumed that these "cutting-off" points move in a random direction along the network structure of silicate melts. The equation of viscosity  $\eta$  in binary silicate system derived from the above concept in earlier studies 16-21) is given by the following equations:

$$\eta = A \cdot \exp\left(\frac{E_{\rm V}}{RT}\right)$$
....(1)

$$E_{\rm V} = \frac{E}{1 + \sqrt{\alpha \cdot (N_{\rm O^-} + N_{\rm O^{2-}})}} \dots (2)$$

where  $A~(=4.80\times10^{-8})$  is a constant,  $E_{\rm V}$  is the activation energy for viscosity, R is the gas constant, and T is the temperature.  $E~(=5.21\times10^5~({\rm J}))$  is the activation energy for viscosity of pure  ${\rm SiO_2}$ , and  $\alpha$  is the parameter relating to the weakness of the bonding between the cation and oxygen ion at the "cutting-off" point, which depends on the oxide component.  $N_{\rm O^-}$  and  $N_{\rm O^{2-}}$  are fractions of the non-bridging oxygen ion and free oxygen ion, respectively. The  $N_{\rm O^-}$  and  $N_{\rm O^{2-}}$  are evaluated by the IRSID 'cell model'. <sup>22,23)</sup>

In the evaluation of chemical bonds of oxygen, Susa *et al.*<sup>24)</sup> assumed that the structure of the aluminosilicate melts is composed of only three kinds of chemical bonds. Their assumption results in the calculation of chemical bonds of oxygen solely by the concentration of slag components. In addition, by considering the Al–BO bond in their equation, the oxygen states can be estimated in case that aluminum oxide works as network former.



Bridging oxygen

CaO or

Non-bridging oxygen ion

O O • Si ② Ca

Fig. 1. Structure of silicate slag.

The equation to calculate the viscosity of silicate melts is modified to the following equations in order to apply the method of Susa *et al.* instead of the IRSID 'cell model' to the evaluation of the bonding states of oxygen:

$$\eta = A \cdot \exp\left(\frac{E_{\text{V}}}{RT}\right) \dots (3)$$

$$E_{\text{V}} = \frac{E}{1 + \sqrt{\sum_{i} \alpha_{i} \cdot N_{\text{(NBO+FO)}_{i}} + \sum_{i} \alpha_{j \text{ in AI}} \cdot N_{\text{(Al-BO)}_{j}}}} \dots (4)$$

where the activation energy  $E_{\rm V}$  is a function of the sum of the fractions of non-bridging oxygen ion (NBO) and free oxygen ion (FO)  $N_{(NBO+FO)_i}$  and the fraction of the bridging oxygen (BO) in the Al tetrahedral unit  $N_{\text{(Al-BO)}}$ .  $N_{\text{(NBO+FO)}}$  is the same as the  $(N_{\rm O^-} + N_{\rm O^{2-}})$  in Eq. (2).  $\alpha_i$  and  $\alpha_{j\,{\rm in}\,{\rm Al}}$  are parameters. i is the component of melt except SiO<sub>2</sub>, i.e. CaO, MgO FeO,  $K_2O$ ,  $Na_2O$ ,  $Al_2O_3$ , and j is the charge-compensating ion from component i except  $Al_2O_3$ , i.e.  $Ca^{2+}$ ,  $Mg^{2+}$ ,  $Fe^{2+}$ ,  $K^+$  and  $Na^+$ . A and E have the same values in the original equation, i.e.  $4.80 \times 10^{-8}$  and  $5.21 \times 10^{5}$  (J) respectively. It is assumed that there are no differences between non-bridging oxygen ions and free oxygen ions in the respect of the influence of those ions on viscosity. The effect of the bridging oxygen in the Al tetrahedral unit on the activation energy is treated in the same manner as the effect of the non-bridging oxygen by assuming that the bridging oxygen in the Al tetrahedral unit has a somewhat different mobility from that of the bridging oxygen in the Si tetrahe-

The fractions of two kinds of oxygen  $N_{({\rm NBO+FO})_i}$  and  $N_{({\rm Al-BO})_j}$  were calculated with reference of the method of Susa  $et~al.^{24)}$  as follows:

(i) Binary system

(i-1) 
$$a\operatorname{SiO}_2 - b_i(\operatorname{M}_x\operatorname{O}_y)_i \{a + b_i = 1 \text{ (mol)}\}\$$
  
 $((\operatorname{M}_y\operatorname{O}_y)_i = \operatorname{CaO}, \operatorname{MgO}, \operatorname{FeO}, \operatorname{K}_2\operatorname{O} \text{ or Na}_2\operatorname{O}) \text{ system}$ 

The addition of basic oxide to silicate provides non-bridging oxygen ions and free oxygen ions by breaking the Si–O bonds in the network structure of silicate; *i.e.* the number of oxygen bonds not connected to Si increases. When  $b_i$  mol of  $(M_xO_y)_i$  is added to silicate, the number of the bonds of oxygen not connected to Si on basic oxide

 $(M_xO_y)_i \; n_{(O-M)_i}$  is  $2b_i$  mol because 1 mol of  $(M_xO_y)_i$  produces 2 mol of oxygen bonds not connected to Si. The total number of the bonds of oxygen in the system  $a{\rm SiO}_2-b_i(M_xO_y)_i$   $n_{{\rm Total-O}}$  is  $4a+2b_i$  mol. In our model, the ratio of the number of oxygen bonds not connected to Si  $n_{(O-M)_i}$  to the total number of the oxygen bonds in the system  $n_{{\rm Total-O}}$  is treated as the sum of the fractions of non-bridging oxygen ions and free oxygen ions  $N_{({\rm NBO+FO})_i}$ . In case of a binary system, the content of bridging oxygen in the Al tetrahedral  $N_{({\rm Al-BO})_i}$  is zero. Subsequently,

$$N_{\text{(NBO+FO)}_i} = n_{\text{(O-M)}_i} / n_{\text{Total-O}} = b_i / (2a + b_i) \dots (5)$$

$$N_{\text{(Al-BO)}} = 0$$
....(6)

(i-2) 
$$aSiO_2-cAl_2O_3$$
 system  $\{a+c=1 \text{ (mol)}\}$ 

In binary  $SiO_2$ – $Al_2O_3$  system, there is no charge-compensating cation from alkaline oxides and alkaline earth oxides, which requires the formation of Al tetrahedral; as a result,  $Al_2O_3$  works as network modifier such as basic oxides. In the same manner as (i-1), the number of oxygen bonds not connected to  $Sin_{(O-M)i}$  is 6c mol with the addition of c mol  $Al_2O_3$ . The total number of oxygen bonds in the  $aSiO_2$ – $cAl_2O_3$  system  $n_{Total-O}$  is 4a+6c mol. Subsequently,

$$N_{\text{(NBO+FO)}_i} = n_{\text{(O-M)}_i}/n_{\text{Total-O}} = 3c/(2a+3c)....(7)$$

$$N_{\text{(Al-BO)}} = 0$$
....(8)

(ii) Ternary 
$$a SiO_2 - b_i (M_x O_y)_i - c Al_2 O_3$$
 system  $\{a + b_i + c = 1 \text{ (mol)}\}$  ( $(M_x O_y)_i = CaO, MgO, FeO, K_2O \text{ or } Na_2O)$ 

(ii-1) 
$$b_i > c$$

When the amount of basic oxide  $(M_v O_v)_i b_i$  is higher than the amount of aluminum oxide c, it is assumed that aluminum oxide only works as network former since there is a sufficient charge-compensating cation j to produce Al tetrahedral in the melts. The number of oxygen bonds in the Al tetrahedral on cation j  $n_{(O-Al in Al)_j}$  is 8c mol. The number of residual oxygen bonds not connected to Si  $n_{(O-M)i}$  is  $2(b_i-c)$  mol because c mol of oxygen as well as c mol of charge-compensating cation is used for the Al tetrahedral in c mol of Al<sub>2</sub>O<sub>3</sub>. The total number of oxygen bonds in the  $a \text{SiO}_2 - b_i (M_x O_y)_i - c \text{Al}_2 O_3$  system  $n_{\text{Total-O}}$  is  $4a + 2b_i + 6c \text{ mol}$ . In the present model, the ratio of the number of oxygen bonds in the Al tetrahedral  $n_{\mathrm{O-Al\,in\,Al}}$  to the total number of oxygen bonds in the system  $n_{\rm Total-O}$  is considered to be the content of the bridging oxygen in Al tetrahedral  $N_{\rm (Al-BO)}$ . Subsequently,

$$N_{\text{(Al-BO)}} = n_{\text{(O-Al in Al)}} / n_{\text{Total-O}} = 4c/(2a + b_i + 3c)......(9)$$

$$N_{\text{(NBO+FO)}_i} = n_{\text{(O-M)}i}/n_{\text{Total-O}} = (b_i - c)/(2a + b_i + 3c) \dots (10)$$

# (ii-2) $b_i < c$

When the amount of basic oxide  $(M_x O_y)_i b_i$  is lower than the amount of aluminum oxide c, it is assumed that basic oxide is used only as charge-compensating ion for the Al tetrahedral. Therefore, the number of oxygen bonds in the Al tetrahedral  $n_{(O-Al\,\text{in}\,\text{Al})_i}$  is  $8b_i$  mol because 1 mol of basic oxide selected in this study results in 2 mol of Al tetrahedral, *i.e.* 8 mol of oxygen bonds in the Al tetrahedral. The number of residual oxygen bonds not connected to Si  $n_{(O-M)_i}$  is  $6(c-b_i)$  mol. This is the number of oxygen bonds pro-

duced from aluminum oxide except for the oxygen bonds in the Al tetrahedral. Therefore,

$$N_{\text{(Al-BO)}_j} = n_{\text{(O-Al in Al)}_j} / n_{\text{Total-O}} = 4b_i / (2a + b_i + 3c) \dots (11)$$

$$N_{\text{(NBO+FO)}_i} = n_{\text{(O-M)}_i} / n_{\text{Total-O}} = 3(c - b_i) / (2a + b_i + 3c) .....(12)$$

(iii) Multi-component 
$$a \text{SiO}_2 - \sum_i b_i (M_x O_y)_i - c \text{Al}_2 O_3$$
 system  $\{a + \sum_i b_i + c = 1 \text{ (mol)}\}\$  ((M<sub>x</sub>O<sub>y</sub>)<sub>i</sub>=CaO, MgO, FeO, K<sub>2</sub>O or Na<sub>2</sub>O)

(iii-1) 
$$\sum_{i} b_{i} > c$$

When the sum of the amount of basic oxide  $(M_xO_y)_i\sum_ib_i$  is higher than the amount of aluminum oxide c, aluminum oxide works only as network former since there is a sufficient charge-compensating cation to produce the Al tetrahedral in the melt as mentioned above. Here, it is assumed that the supply of charge-compensating ions in each basic oxide is proportional to the content of basic oxide, meaning that the number of oxygen bonds in the Al tetrahedral  $n_{(O-Al \, \text{in} \, Al)_j}$  with the charge-compensating cation j is  $8c(b_i/\sum_ib_i)$  mol and that the number of the bonds of oxygen not connected to Si is  $2b_i-2c(b_i/\sum_ib_i)$  mol. Subsequently,

$$N_{\text{(Al-BO)}_{j}} = n_{\text{(O-Al in Al)}_{j}} / n_{\text{Total-O}}$$

$$= 4c \left( b_{i} / \sum_{i} b_{i} \right) / \left( 2a + \sum_{i} b_{i} + 3c \right) \dots (13)$$

$$N_{\text{(NBO+FO)}_{i}} = n_{\text{(O-M)}_{i}} / n_{\text{Total-O}}$$

$$= \left\{ b_{i} - c \left( b_{i} / \sum_{i} b_{i} \right) \right\} / \left( 2a + \sum_{i} b_{i} + 3c \right)$$
.....(14)

(iii-2) 
$$\sum_i b_i < c$$

When the sum of the amount of basic oxide  $(M_xO_y)_ib_i$  is lower than the amount of aluminum oxide c, the equation is derived in the same manner as the equation in the ternary system. Subsequently,

$$N_{\text{(Al-BO)}_j} = n_{\text{(O-Al in Al)}_j} / n_{\text{Total-O}} = 4b_i / \left(2a + \sum_i b_i + 3c\right)$$
.....(15

$$N_{\text{(NBO+FO)}_{i}} = n_{\text{(O-M)}_{i}} / n_{\text{Total-O}}$$

$$= 3 \left( c - \sum_{i} b_{i} \right) / \left( 2a + \sum_{i} b_{i} + 3c \right) \dots (16)$$

# 3. Results and Discussion

# 3.1. Determination of Parameters

There are two kinds of parameters,  $\alpha_i$  and  $\alpha_{j\,\text{in}\,\text{Al}}$ , in the present equation (4) for expressing the viscosity of molten aluminosilicates. The former parameter relates to the non-bridging oxygen ion and the free oxygen ion, and the latter is the parameter relating to the bridging oxygen in the Al tetrahedral. The  $\alpha_i$  and  $\alpha_{j\,\text{in}\,\text{Al}}$  relate to the weaknesses in the bonds of non-bridging oxygen ion, and the weakness of bridging oxygen in the Al tetrahedral, respectively. In the present equation, therefore, the larger parameter values lead to a lower viscosity. These weaknesses of  $\alpha_i$  and  $\alpha_{j\,\text{in}\,\text{Al}}$  depend on the cation next to the non-bridging oxygen ion and

the free oxygen ion, which is the cation produced by the addition of basic oxide  $(M_xO_y)_i$  to silicate, and the charge-compensating cation near Al tetrahedral, which is also the cation produced by adding basic oxide  $(M_xO_y)_i$  to silicate, respectively.

In this study, the parameters  $lpha_i$  and  $lpha_{j\,\mathrm{in}\,\mathrm{Al}}$  were determined from experimental data in binary silicate systems<sup>25–34)</sup> and ternary aluminosilicate systems.<sup>26,34–36,39–41)</sup> The way to determine the parameters is as follows: (i) First, the value of  $\alpha_i$  in each oxide i was obtained from the application of the above equation to fit the experimental values of the viscosity in each binary  $SiO_2$ – $(M_xO_y)_i$  system, where (M<sub>2</sub>O<sub>2</sub>), is CaO, MgO, FeO, K<sub>2</sub>O, Na<sub>2</sub>O or Al<sub>2</sub>O<sub>3</sub>. (ii) Subsequently, the assessment of the value  $lpha_{j\,\mathrm{in}\,\mathrm{Al}}$  in each chargecompensating cation j was conducted by fitting the calculated viscosity with parameter  $\alpha_i$  determined in the binary system to the experimental data in each ternary  $SiO_2-(M_vO_y)_i-Al_2O_3$  system, where  $(M_vO_y)_i$  is CaO, MgO, FeO, K<sub>2</sub>O or Na<sub>2</sub>O. The experimental data<sup>25-41)</sup> used for the determination of these parameters are shown in Table 1, and the assessed parameters are listed in **Table 2**.

# 3.2. Calculation Results

At first, the ability of the present model to represent viscosity using the evaluation manner for oxygen state with reference to Susa *et al.*'s model<sup>24)</sup> was examined by comparing the calculated values with the literature data, which were used for the parameter determinations.

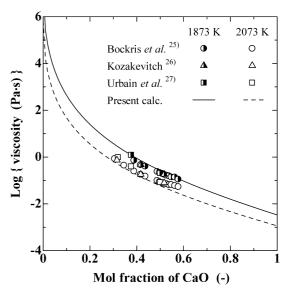
**Table 1.** Experimental data used for determining model parameters.

|         | System   |             | References |
|---------|--|-------------|------------|
| Binary  | SiO <sub>2</sub> -CaO  | 1723 - 2373 | 25-27      |
|         | SiO <sub>2</sub> -MgO  | 1823 - 2273 | 27,28      |
|         | SiO <sub>2</sub> -FeO  | 1473 - 1723 | 29-32      |
|         | SiO <sub>2</sub> -K <sub>2</sub> O                                 | 1373 - 1973 | 28,33      |
|         | SiO <sub>2</sub> -Na <sub>2</sub> O                                | 1373 - 1973 | 28,33      |
|         | SiO <sub>2</sub> -Al <sub>2</sub> O <sub>3</sub>                   | 1973 - 2373 | 26,34      |
| Ternary | SiO <sub>2</sub> -CaO-Al <sub>2</sub> O <sub>3</sub>               | 1423 - 2273 | 26,35      |
|         | SiO <sub>2</sub> -MgO-Al <sub>2</sub> O <sub>3</sub>               | 1673 - 2073 | 36-39      |
|         | SiO <sub>2</sub> -FeO-Al <sub>2</sub> O <sub>3</sub>               | 1523 - 1573 | 40         |
|         | SiO <sub>2</sub> -K <sub>2</sub> O-Al <sub>2</sub> O <sub>3</sub>  | 1523 - 1673 | 39         |
|         | SiO <sub>2</sub> -Na <sub>2</sub> O-Al <sub>2</sub> O <sub>3</sub> | 1523 - 1773 | 41         |

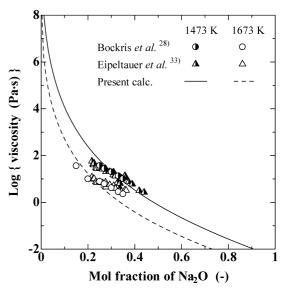
Table 2. Model parameters.

| $(\mathbf{M}_{\mathbf{x}}\mathbf{O}_{\mathbf{y}})_i$ | $lpha_i$ | j                  | $a_{j \text{ in Al}}$ |
|--|----------|--------------------|-----------------------|
| CaO  | 4.00     | Ca <sup>2+</sup>   | 1.46                  |
| MgO  | 3.43     | $\mathbf{Mg}^{2+}$ | 1.56                  |
| FeO  | 6.05     | $Fe^{2+}$          | 3.15                  |
| $K_2O$   | 6.25     | $\mathbf{K}^{+}$   | -0.69                 |
| Na <sub>2</sub> O                                    | 7.35     | $\mathbf{Na}^+$    | 0.27                  |
| $Al_2O_3$  | 1.14     |                    |                       |

The calculation results with the experimental data in binary systems, SiO<sub>2</sub>-CaO, SiO<sub>2</sub>-Na<sub>2</sub>O and SiO<sub>2</sub>-Al<sub>2</sub>O<sub>3</sub>, are shown in **Figs. 2–4**. The present model represents the com-



**Fig. 2.** Viscosity of SiO<sub>2</sub>–CaO system.



**Fig. 3.** Viscosity of SiO<sub>2</sub>–Na<sub>2</sub>O system.

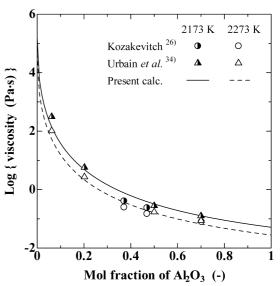
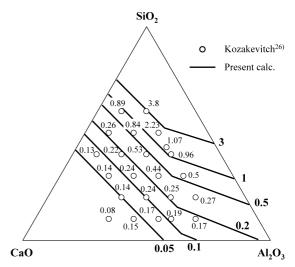


Fig. 4. Viscosity of SiO<sub>2</sub>-Al<sub>2</sub>O<sub>3</sub> system.

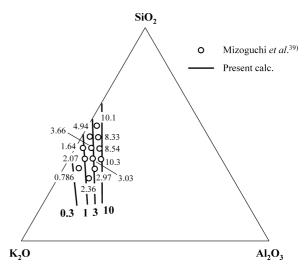
position dependences of viscosity in these binary systems. The calculated values tend to deviate slightly downward from the experimental values with higher CaO and Na2O contents in SiO<sub>2</sub>-CaO and SiO<sub>2</sub>-Na<sub>2</sub>O systems. This deviation could be due to the assumption that there are no differences between the influence of non-bridging oxygen ions and free oxygen ions on viscosity. In the previous studies, 16-21) the content of non-bridging oxygen ion and the content of free oxygen ion were individually calculated by the IRSID 'cell model', and the sum of these oxygen contents described the composition dependence of viscosity over a wide composition range. The thermodynamically calculated  $(N_{O^-}+N_{O^{2-}})$  in a binary system, for example, increases until a certain composition, and then does not change so much. This behavior corresponds to the composition dependence of viscosity in binary systems, which shows a sharp decrease in viscosity in the range from pure SiO<sub>2</sub> to a certain composition, after which the viscosity decreases only slightly. In the present model, on the other hand, the sum of the fractions of non-bridging oxygen ions and free oxygen ions  $N_{(NBO+FO)_i}$  was estimated only from the number of all oxygen bonds not connected to Si except for the bonds in Al tetrahedral, leading to a continuous increase of  $N_{({\rm NBO+FO})_i}$  with increasing the basic oxide in the whole composition range, i.e. the viscosity continues to decrease to some extent even at higher basic oxide content.

Figures 5 and 6 show the viscosities in ternary aluminosilicate systems, SiO<sub>2</sub>-CaO-Al<sub>2</sub>O<sub>3</sub> at 1973 K and SiO<sub>2</sub>-K<sub>2</sub>O-Al<sub>2</sub>O<sub>3</sub> at 1 673 K, respectively. In these figures, the lines are the iso-viscosities calculated by the present model and the dots represent experimental data. The isoviscosity line breaks at a certain point in Fig. 5. This is the point in which the content of CaO is equal to the content of Al<sub>2</sub>O<sub>3</sub> in mol. When the amount of CaO is higher than the amount of aluminum oxide, aluminum oxide works only as network former due to a sufficient amount of charge-compensating ion Ca<sup>2+</sup> for producing the Al tetrahedral in the melts as mentioned above. On the other hand, at the Al<sub>2</sub>O<sub>3</sub> side of the above point, aluminum oxide works as network modifier as well as network former because of the lack of charge-compensating ion Ca<sup>2+</sup>. The iso-viscosity lines calculated relating to this point by the present model describe the composition dependency of experimental viscosity over a wide composition region in the SiO<sub>2</sub>-CaO-Al<sub>2</sub>O<sub>3</sub> system at 1973 K, although the calculated results show a slightly lower viscosity than the experimental data at low SiO2 contents, as well as in binary systems. In Fig. 6, the calculation results in SiO<sub>2</sub>-K<sub>2</sub>O-Al<sub>2</sub>O<sub>3</sub> at 1673 K are in agreement with the experimental data although the composition region targeted in the present calculation is narrow.

The viscosity in quaternary aluminosilicate slags containing MgO or FeO was shown in **Figs. 7** and **8**. Figure 7 presents the viscosity of SiO<sub>2</sub>–CaO–MgO–10mass%Al<sub>2</sub>O<sub>3</sub> slag at 1 723 K. The calculated iso-viscosity lines well express the composition dependency in viscosity measured by Machin *et al.*, <sup>42,43)</sup> showing the lowering of viscosity with decreasing SiO<sub>2</sub>. The viscosity in quasi-ternary SiO<sub>2</sub>–CaO–FeO system at 20mass%Al<sub>2</sub>O<sub>3</sub> by Gimmelfarb<sup>44)</sup> indicates an unusual trend in Fig. 8, where the viscosity decreases by increasing CaO or FeO at relatively high SiO<sub>2</sub> content, and more CaO or FeO yields the increase in viscosity. As can be



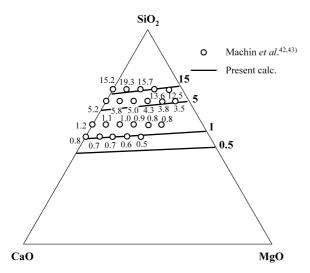
**Fig. 5.** Viscosity (Pa·s) of SiO<sub>2</sub>–CaO–Al<sub>2</sub>O<sub>3</sub> system (mass%) at 1 973 K.



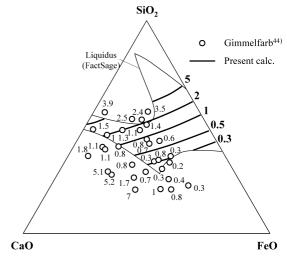
**Fig. 6.** Viscosity (Pa·s) of SiO<sub>2</sub>–K<sub>2</sub>O–Al<sub>2</sub>O<sub>3</sub> system (mass%) at 1 673 K.

appreciated from the liquidus line drawn with "FactSage" in this figure, the data at low  ${\rm SiO_2}$  concentration exist in the zone of coexistence of solid and liquid, leading to a viscosity rise. Comparing the calculated viscosity with the literature data in a liquid region, it was found that the present model reproduces the viscosities in  ${\rm SiO_2-CaO-MgO-10mass\%Al_2O_3}$  system.

Finally, the prediction of viscosity in the quaternary aluminosilicate system SiO<sub>2</sub>–CaO–Al<sub>2</sub>O<sub>3</sub>–K<sub>2</sub>O or Na<sub>2</sub>O was attempted by using the present model. The viscosity measurements of the molten aluminosilicates containing alkali oxide have been conducted by the group of Nakashima *et al.*<sup>45)</sup> **Figure 9** shows the viscosity of quaternary aluminosilicate melts SiO<sub>2</sub>–CaO–Al<sub>2</sub>O<sub>3</sub>–K<sub>2</sub>O or Na<sub>2</sub>O at 1 873 K. Figure 9(a) shows the measured viscosity, whose values were taken from data points from Ref. 45), and Fig. 9(b) shows the calculated values by the present model. In Figs. 9(c) and 9(d), in addition, the calculations were conducted by the two generally-known models, (i) Riboud model<sup>46)</sup> and (ii) modified Iida model,<sup>47)</sup> which can be applied to the aluminosilicate systems containing alkaline oxides and have been recognized as models suited for estimating the



**Fig. 7.** Viscosity (Pa·s) of SiO<sub>2</sub>–CaO–MgO–10Al<sub>2</sub>O<sub>3</sub> system (mass%) at 1723 K.



**Fig. 8.** Viscosity (Pa·s) of SiO<sub>2</sub>–CaO–FeO–20Al<sub>2</sub>O<sub>3</sub> system (mass%) at 1 623 K.

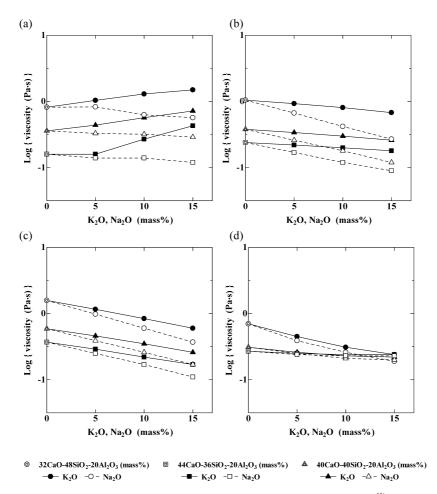


Fig. 9. Viscosity of SiO<sub>2</sub>—CaO—Al<sub>2</sub>O<sub>3</sub>—K<sub>2</sub>O or Na<sub>2</sub>O system at 1 873 K. (a) Experimental data, <sup>45)</sup> (b) present calculation, (c) Riboud model <sup>46)</sup> and (d) modified Iida model. <sup>47)</sup>

viscosity of industrial slags. <sup>48)</sup> In Fig. 9(a), the viscosity of SiO<sub>2</sub>–CaO–Al<sub>2</sub>O<sub>3</sub>–K<sub>2</sub>O melts increases with increasing the content of K<sub>2</sub>O, while the viscosity of SiO<sub>2</sub>–CaO–Al<sub>2</sub>O<sub>3</sub>–Na<sub>2</sub>O melts decreases with increasing content of Na<sub>2</sub>O. On the other hand, the addition of Na<sub>2</sub>O to molten SiO<sub>2</sub>–CaO–Al<sub>2</sub>O<sub>3</sub>–Na<sub>2</sub>O system lowers the viscosity, and the viscosity in SiO<sub>2</sub>–CaO–Al<sub>2</sub>O<sub>3</sub>–K<sub>2</sub>O indicates a slight decrease with the addition of K<sub>2</sub>O in the calculation of the results in Fig. 9(b). As shown in Fig. 9(c), Riboud model has a simi-

lar trend as the present model, but with stronger decreasing influence on viscosity by increasing  $K_2O$  or  $Na_2O$  than the present model. In the calculation results of modified Iida model in Fig. 9(d), the additions of  $K_2O$  and  $Na_2O$  yield a similar composition dependence of viscosity. From this result, it was found that the present model clearly expresses the difference between the effect of  $K_2O$  addition and the effect of  $Na_2O$  addition to  $SiO_2$ –CaO– $Al_2O_3$  melts on viscosity in comparison with the other models, although the

calculation values don't describe the increment of viscosity of adding K<sub>2</sub>O. In the present model, the following two parameters determine the behavior of viscosity with varying composition in aluminosilicate system: (i) the parameter  $\alpha_{iin Al}$ , which was introduced as the weakness of bridging oxygen in the Al tetrahedral with charge-compensating cation j, and (ii) the amount of each charge-compensating ion supplied to form Al tetrahedral. In the former case, the  $\alpha_{j \text{in Al}}$  of  $K_2O$  is smaller than the  $\alpha_{j \text{in Al}}$  of  $Na_2O$ , which means the bond of bridging oxygen in the Al tetrahedral with K<sup>+</sup> is stronger than Na<sup>+</sup>. The calculated results in two quaternary systems SiO<sub>2</sub>-CaO-Al<sub>2</sub>O<sub>3</sub>-K<sub>2</sub>O and SiO<sub>2</sub>-CaO- $Al_2O_3$ - $Na_2O$  reflect the parameter  $\alpha_{j \text{ in Al}}$ . In the latter case, it is reasonable to suppose that some of cations preferentially or with higher possibility work as charge-compensating ion since each cation has specific properties like interactions with other ions. Due to a lack of this information, however, in this study it was assumed that the supply of charge-compensating ion from each basic oxide was proportional to the content of basic oxide, which causes a poor reproducibility of composition dependence of experimental values in SiO<sub>2</sub>-CaO-Al<sub>2</sub>O<sub>3</sub>-K<sub>2</sub>O system. For example, if K<sup>+</sup> works as charge-compensating ion strongly in comparison with Ca<sup>2+</sup>, i.e. the amount of K<sup>+</sup> as charge-compensating ion is larger than that estimated with the present assumption and the amount of Ca<sup>2+</sup> is smaller, the viscosity is higher than the viscosity calculated in the present work since  $\alpha_{i \text{ in Al}}$  of K<sup>+</sup> is smaller than  $\alpha_{i \text{ in Al}}$  of Ca<sup>2+</sup>. As a result, this gives a better description of viscosity in SiO<sub>2</sub>-CaO-Al<sub>2</sub>O<sub>3</sub>-K<sub>2</sub>O system.

# 4. Conclusions

The earlier viscosity model derived by considering the bonding states of oxygen in molten silicate slag and its flow mechanism was modified in order to estimate the viscosity of aluminosilicate melts including alkali oxides. In this modification, the concentration of non-bridging oxygen ions and free oxygen ions used in the calculation of bonding states of oxygen were evaluated with reference to the method of Susa *et al.* instead of a thermodynamic model. The present model can present the composition dependence of viscosity in ternary aluminosilicate systems as well as quaternary aluminosilicate systems containing MgO or FeO, and the distinction of the effects of K<sub>2</sub>O and Na<sub>2</sub>O on viscosity in quaternary aluminosilicate systems containing each alkali oxide without thermodynamic parameters.

#### **REFERENCES**

- Y. Miyabayashi, T. Yoshikawa and T. Tanaka: J. High Temp. Soc., 32 (2006), 281.
- 2) T. Aoki, K. Miyamoto and Y. Kawasaki: Patent, JP, 2003-181412, A.
- 3) J. Hino and Y. Miyabayashi: J. High Temp. Soc., 25 (1999), 59.
- Y. Miyabayashi, H. Noto and M. Narisako: J. Min. Mater. Process. Int. Jpn., 121 (2005), 149.
- T. Aoki, Y. Miayabayashi and T. Yanagida: *J. Min. Mater. Process. Int. Jpn.*, **122** (2006), 235.
- K. C. Mills, L. Chapman, A. B. Fox and S. Sridhar: Scand. J. Metall., 30 (2001), 396.
- 7) A. Kondratiev, E. Jak and P. C. Hayes: JOM, 54 (2002), 41.
- S. Seetharaman, K. Mukai and D. Sichen: Proc. 7th Int. Conf. on Molten Slags, Fluxes and Salts, SAIMM, Johannesburg, (2004), 31.

- L. Zhang and S. Jahanshahi: Metall. Mater. Trans. B, 29B (1998), 177
- L. Zhang and S. Jahanshahi: *Metall. Mater. Trans. B*, **29B** (1998), 187.
- L. Zhang and S. Jahanshahi: Proc. 7th Int. Conf. on Molten Slags, Fluxes and Salts, SAIMM, Johannesburg, (2004), 51.
- A. Kondratiev and E. Jak: Proc. 7th Int. Conf. on Molten Slags, Fluxes and Salts, SAIMM, Johannesburg, (2004), 141.
- 13) A. Kondratiev, P. C. Hayes and E. Jak: ISIJ Int., 46 (2006), 359.
- 14) A. Kondratiev, P. C. Hayes and E. Jak: ISIJ Int., 46 (2006), 368.
- 15) A. Kondratiev, P. C. Hayes and E. Jak: ISIJ Int., 46 (2006), 375.
- T. Tanaka, M. Nakamoto and T. Usui: Proc. of Japan–Korea Workshop on Science and Technology in Ironmaking and Steelmaking, ISIJ, Tokyo, (2003), 56.
- T. Tanaka, M. Nakamoto, J. Lee and T. Usui: Proc. of Science and Technology of Innovative Ironmaking for Aiming at Energy Half Consumption, MEXT, Tokyo, (2003), 161.
- T. Tanaka, M. Nakamoto and J. Lee: Proc. of Metal Separation Technologies III, Symp. in Honor of Professor Lauri E. Holappa, HUT, Espoo, (2004), 135.
- T. Tanaka, M. Nakamoto, K. Nakashima and N. Saito: Proc. of Australia–Japan Iron & Steelmaking Symposium, UNSW, Sydney, (2004), 1.
- M. Nakamoto, T. Tanaka, J. Lee and T. Usui: ISIJ Int., 44 (2004), 2115.
- 21) M. Nakamoto, J. Lee and T. Tanaka: ISIJ Int., 45 (2005), 651.
- H. Gaye and J. Welfringer: Proc. 2nd Int. Symp. Metall. Slags and Fluxes, Met. Soc. of AIME, Warrendale, PA, (1984), 357.
- H. Gaye and J. Lehmann: Proc. 7th Int. Conf. on Molten Slags, Fluxes and Salts, SAIMM, Johannesburg, (2004), 619.
- M. Susa, Y. Kamijo, K. Kusano and R. Kojima: Glass Technol., 46 (2005), 55.
- J. O'M. Bockris and D. C. Lowe: Proc. R. Soc. (London), 226A (1954), 423.
- 26) P. Kozakevitch: Rev. Metall., 57 (1960), 149.
- 27) G. Urbain: Rev. Int. Hautes Temp. Refract., 11 (1974), 133.
- J. O'M Bockris, J. D. Mackenzie and J. A. Kitchener: Trans. Faraday Soc., 57 (1955), 1734.
- 29) P. Kozakevitch: Rev. Metall., 46 (1949), 505.
- P. Roentgen, H. Winterhager and L. Kammel: Z. Erz. Metall., 9 (1956), 207.
- T. Myslivec, J. Wozniak and V. Cerny: Sb. Ved. Pr. Vys. Sk. Banaske Ostrave, 20 (1974), 57.
- G. Urbain, Y. Bottinga and P. Richet: Geochim. Cosmochim. Acta, 46 (1982), 1061.
- 33) E. Eipeltauer and G. Jangg: Kolloidn. Zh., 142 (1955), 77.
- 34) G. Urbain: Rev. Int. Hautes Temp. Reflect., 20 (1983), 135.
- J. S. Machin, T. B. Yee and D. L. Hanna: J. Am. Ceram. Soc., 35 (1952), 322.
- R. A. Lyutikov and L. M. Tsylev: Izv. Akad. Nauk SSSR, Otd. Tekh. Nauk, Metall. Gorn. Delo, (1963), 41.
- 37) E. F. Riebling: Can. J. Chem., 42 (1964), 2811.
- 38) G. Hofmaier: Berg Huttenman. Monatsh., 113 (1968), 269.
- K. Mizoguchi, K. Okamoto and Y. Suginohara: J. Jpn. Inst. Met., 46 (1982), 1055.
- P. Rontgen, H. Winterhager and R. Kammel: Erzmetall, 9 (1956), 207.
- T. Kou, T. Mizoguchi and Y. Suginohara: J. Jpn. Inst. Met., 42 (1978), 775.
- J. S. Machin, T. B. Yee and D. L. Hanna: J. Am. Ceram. Soc., 35 (1952), 322.
- 43) J. S. Machin and T. B. Yee: *J. Am. Ceram. Soc.*, **37** (1954), 177.
- 44) A. A. Gimmelfarb: Izv. Akad. Nauk SSSR Metally, (1968), 59.
- S. Sukenaga, N. Saito, K. Kawakami and K. Nakashima: *ISIJ Int.*, 46 (2006), 352.
- P. V. Riboud, Y. Roux, L.-D. Lucas and H. Gaye: Fachber: Httenprax. Metallweiterverab., 19 (1981), 859.
- T. Iida, H. Sakai, Y. Kita and K. Murakami: *High Temp. Mater. Proc.*, 19 (2000), 153.
- K. C. Mills, A. B. Fox, L. Chapman and S. Sridhar: Scand. J. Metall., 30 (2001), 396.